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Lazhar, Ramzi and Najjari, Mustapha and Prat, Marc *Combined wicking and evaporation of NaCl solution with efflorescence formation: The efflorescence exclusion zone*. (2020) *Physics of Fluids*, 32 (6). 067106. ISSN 1070-6631

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# Combined wicking and evaporation of NaCl solution with efflorescence formation: The efflorescence exclusion zone

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## ABSTRACT

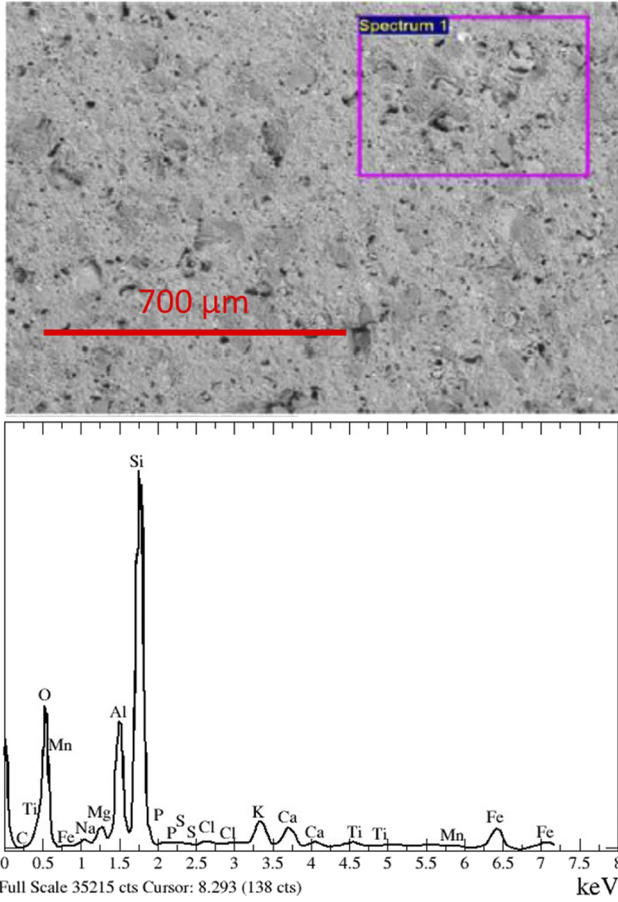
An experiment combining wicking and evaporation of a NaCl solution and leading to the formation of salt efflorescence is presented. The experiment shows that efflorescence develops over the porous medium surface exposed to evaporation except in the bottom region of the sample. This region remains free of efflorescence and is called the exclusion zone. It is shown that the exclusion zone extent depends on the solute concentration in the bottom reservoir. A model is developed, and it helps understand the exclusion phenomenon. The arch shape of the exclusion zone upper boundary is explained and modeled. The study is also seen as a successful test for the model of efflorescence growth driven by evaporation and salt precipitation presented in a previous study. The modeling approach is expected to help develop better models of salt transport with crystallization at the surface of porous media in relation with soil salinization issues or the salt weathering of porous materials.

<https://doi.org/10.1063/5.0007548>

## 1. INTRODUCTION

Crystallization of salt in porous media is one of the major causes of the damage both in cultural heritage and in civil engineering constructions. Also, salt crystallization at the surface of a soil can severely affect evaporation and, thus, soil-atmosphere exchange. These applications have motivated quite a few works, e.g., Refs. 1–7, to name only a few. Modeling this type of situation implies dealing with the trio: evaporation, ion transport in solution within a porous medium, and crystallization. Despite the significance of the aforementioned applications and the numerous publications, developing predictive models and validating them against experimental data are still largely an open question, at least when a significant crystallization takes place. In this respect, it is convenient to distinguish two main situations as discussed, for instance, in Ref. 8: drying and evaporation-wicking. Consider an initially wet porous sample. Drying<sup>9,10</sup> is typically when there is no supply in solution during evaporation. In contrast, evaporation-wicking<sup>11</sup> is when the solution can be sucked, typically by the capillary effect, into the sample

so as to compensate, at least partly, the evaporation. As discussed in Ref. 11, the sample can actually stay fully saturated when the solution absorption rate fully compensates the evaporation. In what follows, we are interested in this situation. Hence, the material will be saturated all the time. In practice, this situation can be encountered where a construction is in contact with natural groundwater or in a marine environment. A well-known example is the constructions in the city of Venice. The situation before the onset of crystallization is less tricky, and reasonably reliable models can be used to predict the ion distribution within a porous sample exposed to evaporation. In the case of the evaporation-wicking situation, one can refer, for instance, to Ref. 11, where it is shown that using the standard macroscopic convection-diffusion equation for the ion transport leads to fairly good results. The solution developed in Ref. 11 corresponds to a quasi-1D situation where evaporation occurs only at the top surface of the sample, the solution is supplied through the sample bottom surface, and the sample lateral sides are impervious. We consider the somewhat different situation where evaporation takes place not only at the top surface but also along the lateral sides. This is



**FIG. 1.** SEM-EDS analysis of the surface ceramic. Top: SEM image perpendicular to the sample surface, pores correspond to black spots in the image; bottom: EDS spectrum of the ceramic.

also a classical situation, notably considered in laboratory tests.<sup>12,13</sup> More importantly, we are interested in the situation where a quite significant development of salt (NaCl) crystals takes place. The study combines experiment and modeling. In the experiment, salt efflorescence develops covering a quite significant fraction of the evaporation surface of the porous medium. Interestingly, however, a noticeable fraction of the evaporation surface stays free of efflorescence. This phenomenon is referred to as the exclusion effect. The experiment indicates that the spatial extension of the exclusion zone varies with the solute concentration in the solution reservoir into which

the sample bottom region is plunged. In the present state of the art in the concerned research area, the exclusion zone phenomenon can be seen as an interesting modeling challenge since it is observed in a situation where crystallization is quite significant. In other words, can we understand the exclusion effect and propose a predictive model? In addition to highlighting and describing the efflorescence exclusion effect, answering these questions is the main objective of the present paper. It is organized as follows: The porous material and the experimental setup are described in Secs. II and III, respectively. Experimental results are presented in Sec. IV. Modeling is presented in Sec. V together with comparisons with the experimental results. A short discussion is proposed in Sec. VI. Conclusions are drawn in Sec. VII.

## II. POROUS MATERIAL

The porous medium is a glazed ceramic (Faience tile—Tunisian industry). This material has been used in buildings for decoration of inner and outer walls of private houses, historic monuments, and state buildings. Particle-induced x-ray diffraction (XRD), electron microprobe analysis [energy dispersive spectra (EDS)], and scanning electron microscopy (SEM) analytical techniques were used to characterize the surface of the material. Major, minor, and trace elements were detected by XRD, and SEM-EDS gave information on the main mineral phases. The main mineral of the porous ceramic surface, identified by x-ray diffraction, is the quartz (SiO<sub>2</sub>). The main major chemical elements obtained by SEM-EDS are SiO<sub>2</sub>, CaCO<sub>3</sub>, MgO, Al<sub>2</sub>O<sub>3</sub>, GaP, FeS<sub>2</sub>, and TiO<sub>2</sub>. Therefore, the conclusion is that there is no internal source of NaCl in this material. Figure 1 displays the characteristics of the surface by SEM images and EDS semi-quantitative analyses. Table I shows the chemical composition corresponding to the spectrum shown in Fig. 1.

The porosity accessible to water, denoted by  $\epsilon_{pm}$ , was determined on pieces of ceramic according to the American Technique Standard (ASTM C642-97).<sup>14</sup> This gave  $\epsilon_{pm} \approx 0.2$ . As indicated in Fig. 1, relatively big pores, on the order of a few tens of micrometers, are present.

## III. EXPERIMENTAL SETUP

Five pieces, referred to as A1, A2, A3, A4, and A5, were cut in rectangular shape from a glazed ceramic, keeping the glazed side as one side of the sample. Dimensions of these samples are given in Table II. Initially, all samples were dried. Sample A1 was saturated with pure water. The other samples were contaminated by NaCl by immersion in an aqueous solution. Various salt concentrations were considered as indicated in Table II. When all samples were fully saturated, they were set vertically in reservoirs filled with the

**TABLE I.** Mean percentage of chemical composition of the studied ceramic surface expressed as wt. % and at. % obtained by means of SEM-EDX analysis.

Element	Si	O	Ca	Mg	C	P	S	Ti	Fe	Mn	Al	K
wt. %	27.85	45.11	2.29	1.55	4.27	0.32	0.16	0.50	6.32	0.09	8.06	2.75
at. %	20.55	58.43	1.18	1.32	7.36	0.21	0.10	0.21	2.34	0.03	6.19	1.46

**TABLE II.** Sample geometrical dimensions and initial NaCl concentration for the various samples [see Fig. 2(b) for the notations,  $H_t = H + H_i$ ]. The exclusion length  $H_e$  is the height of the region free of efflorescence at the end of the experiment. As shown in Fig. 6, it is measured in the middle of the front face as the vertical distance between the bottom of the non-immersed part of the sample and the first crystals at the surface. The solubility ion mass fraction is 0.264 (which corresponds to 6.1M).

Sample	Immersion solution (NaCl mass fraction $C_0$ )	$H$ (cm) (external length)	$H_i$ (cm) (immersed length)	$H_t$ (cm) (total length)	$w$ (cm)(width)	$e$ (cm) (thickness)	$H_e$ (cm) (exclusion length)
A1	Pure water	11	5.5	16.5	7.5	0.6	...
A2	0.1	11	5.5	16.5	7.5	0.6	6.5
A3	0.15	11	5.5	16.5	7.5	0.6	5
A4	0.2	11	5.5	16.5	7.5	0.6	3.5
A5	0.25	11	5.5	16.5	7.5	0.6	2

corresponding saturating solution (Fig. 2), i.e., with the composition same as that of the one used to soak the sample. The immersion depth of a sample in the reservoir was 5.5 cm. The presence of the reservoir ensured a continuous supply of the solution to the sample and then compensates the loss of water resulting from evaporation.

As shown in Fig. 2, the upper part of the samples was exposed to evaporation. Note that no relative humidity and temperature control were imposed in the experiment room. Figure 3 shows the relative humidity and temperature variations measured in the experiment room during the experiment. Also, note that the back face of the samples corresponds to the glazed surface. As a result, there was no evaporation from the back face. As sketched in Fig. 2(b), evaporation occurred at the top surface, the front face, and the two lateral faces.

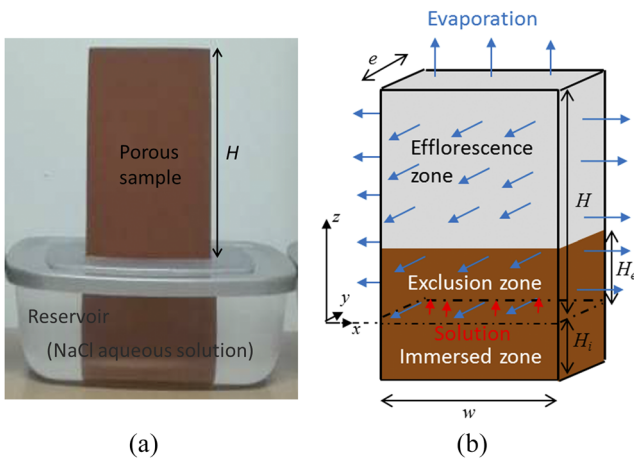
As illustrated in Fig. 2, the reservoirs were well closed except for the opening hole on the top surface used to introduce the sample. Thus, one can consider that the direct evaporation of the solution from the reservoir, if any, was quite limited. The mass loss of each system (sample and reservoir) due to evaporation was measured by using an electronic balance with an accuracy of  $\pm 0.001$  g. The development of the efflorescence and its distribution on the evaporation

surface of the samples were recorded during 10 days using a camera with a resolution of  $4160 \times 2336$  pixels<sup>2</sup>.

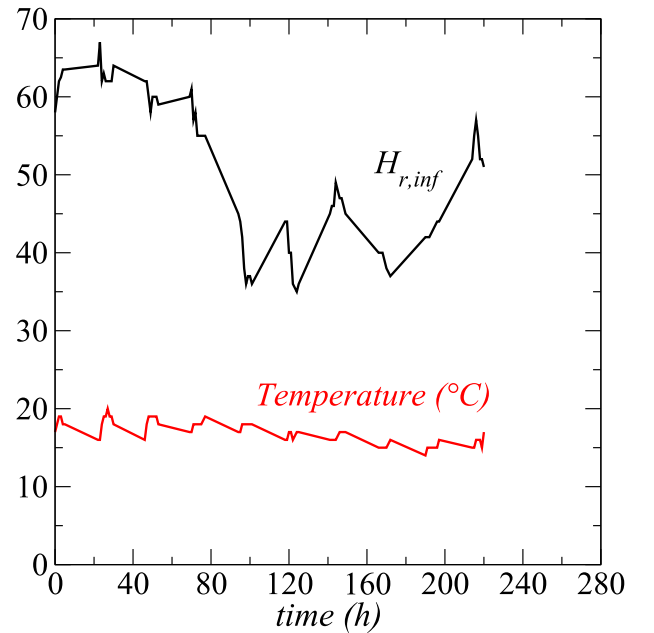
#### IV. EXPERIMENTAL RESULTS

##### A. Salt crystallization dynamics: The efflorescence exclusion zone

Figure 4 shows images of the efflorescence development over the surface at different times for the initial ion mass fraction  $C_0 = 0.25$ . The images actually correspond to a preliminary experiment. The relative humidity and temperature were not recorded in this preliminary experiment, and only two NaCl initial concentrations were considered. For this reason, the experiment was repeated with more NaCl initial concentrations and with the relative humidity and temperature measurements. For the same initial salt mass fraction,



**FIG. 2.** (a) Porous sample partially immersed in the bottom reservoir at the beginning of the experiment and (b) sketch of the studied system with the main notations.



**FIG. 3.** Relative humidity  $H_{r,inf}$  and temperature variations in the experiment room close to the samples over the experiment duration.

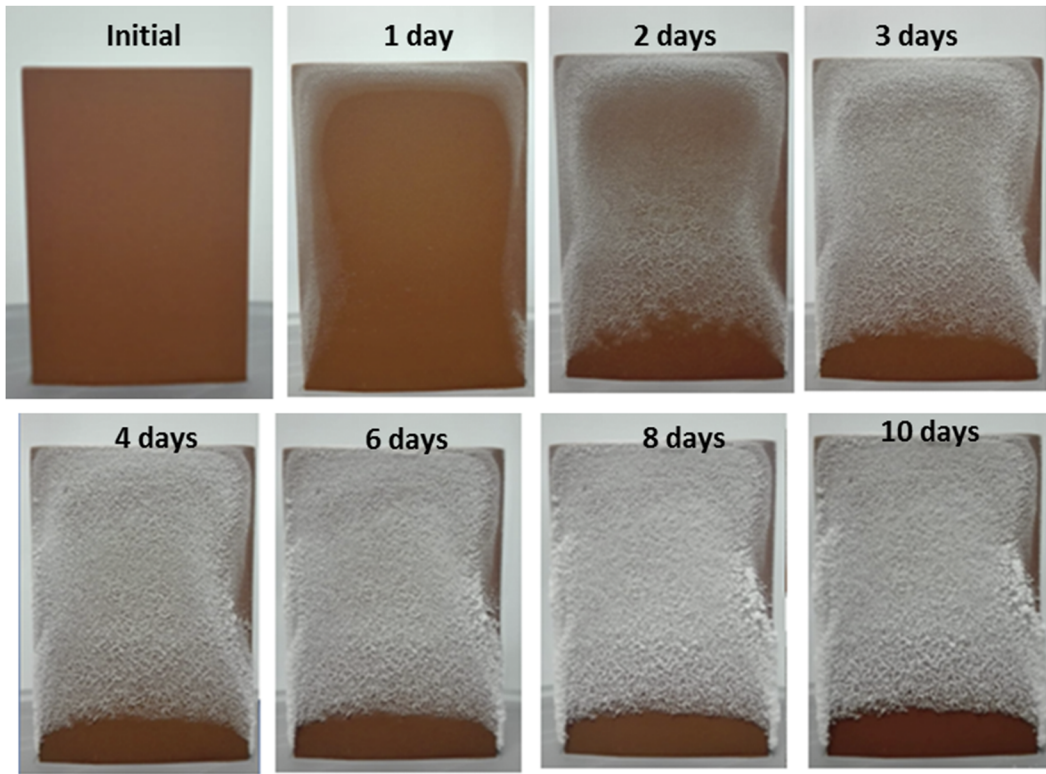


FIG. 4. Typical efflorescence development over the sample surface for  $C_0 = 0.25$ .

both experiments led to the same exclusion zone, which is seen as a good repeatability test. Efflorescence is visible after about one day along the edges of the sample front face. The evaporation flux is expected to be higher at the edges, and it is known that crystallization first occurs where evaporation is greater.<sup>18,19</sup> Actually, as discussed in Sec. V B, the edge effect, i.e., the fact that crystallization begins in the edge regions, can be present even with a uniform evaporation flux due to the combined impact of the evaporation from the front face and from the lateral faces in the edge region. Then, the efflorescence spreads on the evaporation surface, from top to bottom and from the ridges of the sample to the surface middle.

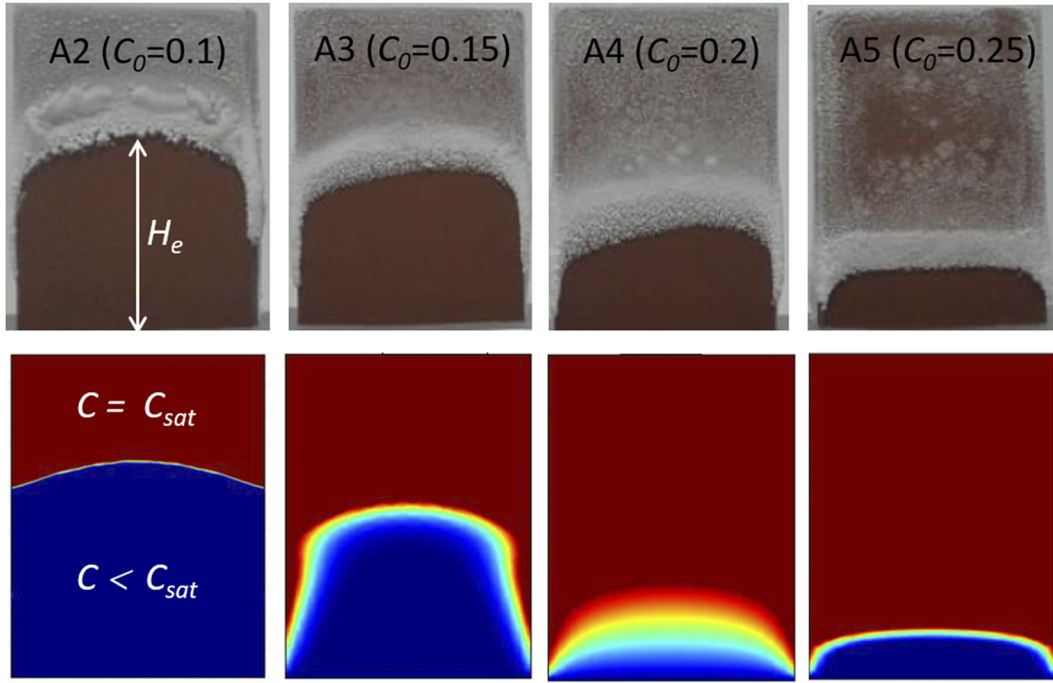
In this example, the surface colonization process takes about one day (compare the image after one day and after two days in Fig. 4). One can wonder whether this surface colonization process has to do with salt creeping,<sup>20</sup> i.e., seen here as the lateral development of the efflorescence from the previous efflorescence salt crystals or simply results from crystallization in new pores at the ceramic surface, as in Ref. 19, for instance, or a mix of both processes. This cannot be deciphered from the data of the present experiment. In any case, it can be seen that the extent of the zone occupied by the efflorescence stabilizes. One can note some additional colonization at the bottom of this zone during the next day (day 3) and that the efflorescence zone gets whiter and whiter, which is a clear indication that the precipitation process continues during the experiment and takes place on top of the efflorescence already in place.

However, the most remarkable and somewhat unexpected fact is that no crystallization of salt is observed during all the experiments in the bottom region of the sample in Fig. 4. This region is referred to as the efflorescence exclusion zone, and the corresponding phenomenon is referred to as the exclusion phenomenon. Since this part of the sample is the closest to the sample immersed part, i.e., to the solute source, one could think that this zone should see the formation of efflorescence. This is clearly not the case. It can be seen that the extent of this zone is quite stable (comparing the image for day ten with the image for day four in Fig. 4). Another interesting feature is the arch shape of its upper boundary, which is interpreted as a consequence of the locally higher evaporation at the edges, due to the contribution of the lateral faces and possibly of a higher external demand in the edge region, compared to the region of the surface away from the edges.

Additional insights on the exclusion zone can be obtained from the images shown in Fig. 5. In particular, it can be seen that the size of the exclusion zone increases when the reservoir ion mass fraction is decreased.

In summary, a quasi-steady state is reached, in which the efflorescence develops over only a fraction of the sample surface exposed to evaporation. The remaining fraction at the bottom is free of efflorescence. The initial NaCl concentration has an impact on the exclusion zone extension. The greater the initial concentration, the lower the extent of the exclusion zone, all other factors being equal.





**FIG. 5.** Top: development of efflorescence over the sample surface at the end of the experiment for the various samples. Impact of the solution concentration in the bottom reservoir. The height of the exclusion zone decreases as the NaCl mass fraction in the reservoir increases. Bottom: efflorescence (in red) and exclusion zone (blue with possible color variations between blue and lighter red) computed using the 2D model described in Sec. VB.

The objective is now to understand and explain these trends from simple modeling considerations. However, some considerations on the evaporation results are necessary beforehand.

### B. Evaporation kinetics

The measured cumulative mass loss  $m_e(t)$  as a function of time for the various samples is shown in Fig. 6.  $m_e(t)$  is computed as

$$m_e(t) = m_0 - m(t), \quad (1)$$

where  $m(t)$  is the mass of the system (sample + reservoir) and  $m_0$  is the mass at  $t = 0$ ;  $m_e(t)$  corresponds to the mass of water leaving the system by evaporation.

The evaporation rate can be computed from these data as follows:

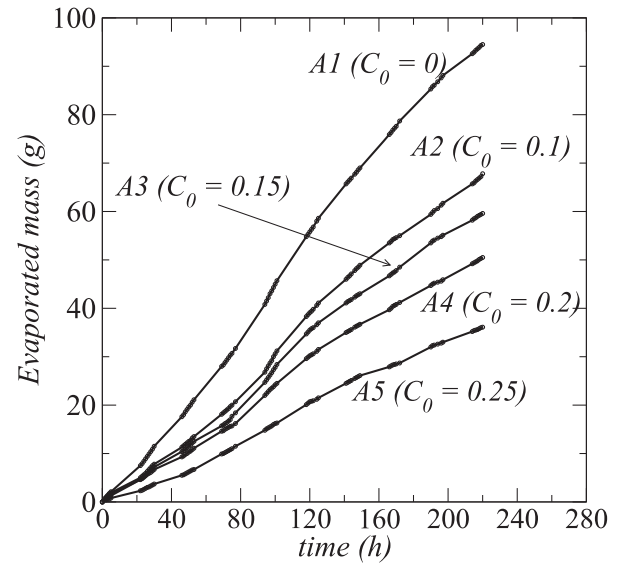
$$J = \frac{dm_e}{dt}. \quad (2)$$

Then, one can determine the mean evaporation flux  $j$  for each porous sample as

$$j = \frac{J}{S} = \frac{1}{S} \frac{dm_e}{dt}, \quad (3)$$

where  $S$  is the total sample surface area open to evaporation. Thus, with the notations indicated in Fig. 2(b),  $S = ew + wH + 2eH$  (it is recalled that there is no evaporation from the sample back face).

As can be seen from Fig. 6, the evaporation rate (the slope of the curves in Fig. 6) does not change very significantly over the duration of the experiment. Since, as discussed before, the formation of efflorescence is quite significant and takes place early in the



**FIG. 6.** Cumulative mass water loss as a function of time for the various samples.

experiment, this is a clear indication that the efflorescence development does not affect very much the evaporation rate. As reported in Refs. 15,16, one can distinguish two main types of efflorescence: blocking and non-blocking. Blocking efflorescence refers to the efflorescence that severely reduces the evaporation rate compared to the evaporation rate before the efflorescence development. It corresponds to the “crusty” efflorescence in Ref. 15. The plot of the evaporated mass as a function of time is characterized in this case by a marked change in the slope of the evaporated mass curve, which tends to become flat. In contrast, the non-blocking efflorescence does not affect very much the evaporation rate, i.e., the slope of the curve  $m_e(t)$  does not vary very much. Thus, referring to this classification, the efflorescence in our experiments can be considered as non-blocking. This corresponds to a porous efflorescence in which the solution is sucked by capillarity up to the efflorescence external surface where water evaporates and salt precipitation makes grow the efflorescence, e.g., Refs. 17, and 18. The slight changes in the slope of the curves in Fig. 6 can be explained by the variation of the relative humidity in the experiment room. As can be seen from Fig. 3, the relative humidity drops after about 80 h. This well corresponds to the increase in the slopes of the curves in Fig. 6, i.e., to an increase in the evaporation rate.

The evaporation rate is typically proportional to the difference between the water vapor partial pressure at the porous sample surface  $p_{vs}$  and the water vapor partial pressure  $p_{vinf.}$  in the room away from the sample:

$$J \propto (p_{vs} - p_{vinf.}). \quad (4)$$

In the case of pure water,  $p_{vs} = p_{vsat}$ , where  $p_{vsat}$  is the saturated water vapor pressure. In the case of the NaCl solution, the solution at the surface is expected to be salt saturated, i.e., at the solubility, at least over the fraction of the surface covered by the efflorescence. The presence of the ions in the solution reduces the water activity. For a saturated NaCl aqueous solution,  $p_{vs} = 0.75p_{vsat}$ . Thus, it is expected that the ratio of the evaporation rate between the pure water saturated sample and the sample A5 for which the ion mass fraction everywhere at the surface can be expected to be close to solubility

(since the ion mass fraction in the reservoir is close to solubility for sample A5) verifies

$$\frac{J_{A1}}{J_{A5}} \approx \frac{(p_{vsat} - p_{vinf.})}{(0.75p_{vsat} - p_{vinf.})} = \frac{(1 - H_{r,inf})}{(0.75 - H_{r,inf})}, \quad (5)$$

where  $H_{r,inf}$  is the relative humidity in the experiment room. With, for instance,  $H_{r,inf} = 0.52$ , which is the average value over the last 24 h period of the experiment (see Fig. 3), one obtains  $\frac{J_{A1}}{J_{A5}} \approx 2$  (as reported in Ref. 15, this ratio is at least one order of magnitude greater when the efflorescence is blocking). Table III shows this ratio computed from the slopes of the  $m_e(t)$  curves over the last 24 h period of the experiment, i.e., between  $t = 196$  h and  $t = 220$  h. As expected,  $\frac{J_{A1}}{J_{A5}} \approx 2$  for sample A5. This ratio is less than 2 for the other samples, i.e., the evaporation rate is closer to the one for pure water. This is consistent with the fact that the ion mass fraction is actually lower than the solubility over a fraction of the sample surface, i.e., the fraction of the surface not covered by the efflorescence. The latter consideration can be further supported by the following estimates. The computation of the ion mass fraction field presented later in the paper indicates that the ion mass fraction field is close to the reservoir ion mass fraction  $C_0$  over most of the surface free of efflorescence. Thus, a more refined estimate of the evaporation rate can be obtained by adding the contribution from the region covered by the efflorescence to the contribution from the region free of efflorescence,

$$J_{Ai} = J_{Ai-free-surface} + J_{Ai-efflorescence}, \quad (6)$$

which leads to

$$J_{Ai} \propto (w + 2e)H_e \frac{M_v}{RT} (p_{vs}(C_0) - p_{vinf.}) + ((w + 2e)(H - H_e) + we) \frac{M_v}{RT} (p_{vs}(C_{sat}) - p_{vinf.}), \quad (7)$$

where  $M_v$  is the vapor molecular weight,  $R$  is the universal gas constant, and  $T$  is the temperature. This leads to

$$\frac{J_{A1}}{J_{Ai}} \approx \frac{((w + 2e)H + we)(p_{vsat} - p_{vinf.})}{(w + 2e)H_e(p_{vs}(C_0) - p_{vinf.}) + ((w + 2e)(H - H_e) + we)(p_{vs}(C_{sat}) - p_{vinf.})}, \quad (8)$$

**TABLE III.** Evaporation rate at the end of experiment for each sample, the evaporation rate ratio (evaporation rate for pure water/evaporation rate for the saline solution), and the Peclet number for the various samples.  $Pe = \frac{V_z(0)H_e}{\varepsilon_{pm}D_s^*}$ , where  $H_e$  is the exclusion height as computed from Eq. (16),  $V_z(0)$  is the filtration velocity at the sample inlet,  $\varepsilon_{pm}$  is the porous medium porosity, and  $D_s^*$  is the solute effective diffusion coefficient in the porous medium.

	A1 ( $C_0 = 0$ )	A2 ( $C_0 = 0.1$ )	A3 ( $C_0 = 0.15$ )	A4 ( $C_0 = 0.2$ )	A5 ( $C_0 = 0.25$ )
$J$ (g/h)	0.278	0.265	0.196	0.2	0.134
$J_{A1}/J_{Ai}$ (from exp. data)	1	1.05	1.4	1.4	2.1
$J_{A1}/J_{Ai}$ [from Eq. (8)]	1	1.4	1.6	1.9	2
$Pe$	...	34	29	25	5

which gives the values reported in Table III (to determine the equilibrium vapor pressure for the different values of the ion mass fraction  $C_0$ , we have used the data presented in Ref. 21). The trend in Table III, i.e., the fact that the evaporation rate ratio decreases as the reservoir ion mass fraction is decreased, is consistent with the fact that the free surface fraction increases as the reservoir ion mass fraction is decreased.

Considering the assumptions and simplifications made, i.e., notably, the fact we have implicitly assumed an uniform external mass transfer coefficient all over the surface, our conclusion is that the comparison between the results from Eq. (8) and the estimates from the experimental data in Table III is sufficiently good for supporting the following main consideration: evaporation takes place all over the surface, i.e., where there is no efflorescence, as well as where the efflorescence is present.

The conclusion is, therefore, that the efflorescence is not blocking in our experiment and that the lower evaporation rate observed with the saline solution is simply due to the lower activity of the solution compared to pure water. Also, the picture is that, in the quasi-steady regime reached by the system, evaporation takes place all over the surface, i.e., the surface fraction free of efflorescence, as well as the surface fraction covered by the efflorescence.

## V. MODELING

### A. Extent of the exclusion zone

Based on the elements discussed in Sec. IV, it is assumed that a quasi-steady regime is reached. Also, the evaporation is little affected by the efflorescence development. Thus, the solution is continuously absorbed by the sample. The ions are transported within the sample up to the surface of the efflorescence where precipitation occurs. If we denote the solute mass flow rate at the sample inlet by  $\phi_{inl.}$  and the precipitation rate at the efflorescence surface by  $\phi_{effl.}$ , then it is expected that  $\phi_{inl.} \approx \phi_{effl.}$ . The latter equality simply means that all the ions entering the sample eventually lead to the formation of new crystals at the external surface of efflorescence. It cannot be excluded that new crystals also form within the efflorescence and/or possibly within the porous sample region adjacent to the efflorescence. However, this is neglected, and we only consider precipitation at the efflorescence external surface. The next step is to express  $\phi_{inl.}$  and  $\phi_{effl.}$ . Throughout the analysis, we assume that the evaporation flux is the same everywhere at the sample evaporation surface and, thus, equal to the mean evaporation flux given by Eq. (3). This is a simplification since it is likely that the evaporation flux varies spatially. To express  $\phi_{effl.}$ , we use the expression of the efflorescence local growth rate  $\varphi$  derived in Ref. 22, namely,

$$\varphi = \frac{C_{sat}(\rho C_{sat}\varepsilon + \rho_{cr}(1 - \varepsilon))}{\rho_{cr}(1 - \varepsilon)(1 - C_{sat})} \left[ \frac{Da}{1 + Da} \right] j, \quad (9)$$

where  $\rho$  is the density of the solution,  $\rho_{cr}$  is the crystal density,  $\varepsilon$  is the efflorescence porosity,  $Da$  is a Damkhöler number characterizing the competition between the precipitation reaction and the diffusive ion transport in the efflorescence, and  $C_{sat}$  is the equilibrium ion mass fraction in a saturated solution ( $C_{sat} = 0.264$ ). In fact, the ion mass fraction on top of the growing efflorescence is greater than  $C_{sat}$  since supersaturation is necessary for the precipitation to occur. However, as discussed in Ref. 10 and also shown in Ref. 22, the supersaturation

is actually very close to the saturation concentration when new crystals form in the presence of already existing crystals. As a result, the approximation  $C \approx C_{sat}$  is made in deriving Eq. (9). One can refer to Refs. 10 and 22 for more details. With the notations in Fig. 2(b), this leads to express  $\phi_{effl.}$  as

$$\phi_{effl.} = ((H - H_e)(w + 2e) + we)\varphi, \quad (10)$$

and, thus, to

$$\phi_{effl.} = ((H - H_e)(w + 2e) + we)\lambda j, \quad (11)$$

where

$$\lambda = \frac{C_{sat}(\rho C_{sat}\varepsilon + \rho_{cr}(1 - \varepsilon))}{\rho_{cr}(1 - \varepsilon)(1 - C_{sat})} \left[ \frac{Da}{1 + Da} \right]. \quad (12)$$

To express the incoming solute mass flow rate, we first note that the velocity induced in the solution as a result of the local evaporation and local efflorescence growth can be expressed according to Ref. 22 as

$$\rho V = (1 + \alpha)j, \quad (13)$$

where

$$\alpha = \frac{C_{sat}(\rho\varepsilon + \rho_{cr}(1 - \varepsilon))}{\rho_{cr}(1 - \varepsilon)(1 - C_{sat})} \left[ \frac{Da}{1 + Da} \right]. \quad (14)$$

Equation (13) applies over the sample external surface where the efflorescence is present. In the exclusion zone, the velocity normal to the surface is simply  $V = \frac{j}{\rho}$ . This leads to express  $\phi_{inl.}$  as

$$\phi_{inl.} = C_0 [((H - H_e)(w + 2e) + we)(1 + \alpha) + H_e(w + 2e)]j - we\rho\varepsilon_{pm}D_s^*B_1, \quad (15)$$

where  $C_0$  is the ion mass fraction in the reservoir,  $\varepsilon_{pm}$  is the porous sample porosity, and  $D_s^*$  is the effective diffusion coefficient of the ions in the porous sample. The factor  $B_1$  comes from the steady-state solution of the convection-diffusion problem in the efflorescence free region located between  $z = 0$  and  $z = H_e$ . Its expression is derived in the Appendix. It notably depends on  $H_e$ .

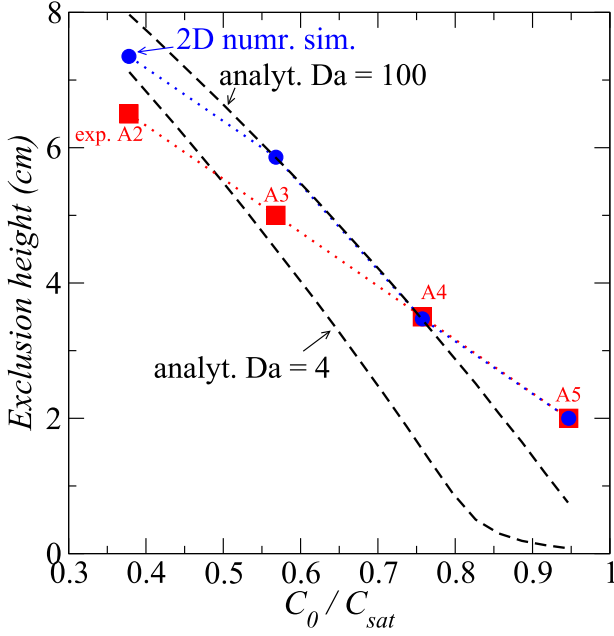
After some algebra, expressing that  $\phi_{effl.} = \phi_{inl.}$  yields

$$H_e - \frac{we}{(w + 2e)} \frac{\rho\varepsilon_{pm}D_s^*B_1}{j(\lambda - C_0\alpha)} = H \left( 1 - \frac{C_0}{(\lambda - C_0\alpha)} \right) + \frac{we}{(w + 2e)} \frac{(\lambda - C_0(1 + \alpha))}{(\lambda - C_0\alpha)}, \quad (16)$$

which is used in what follows to determine the exclusion zone height  $H_e$  as a function of the bottom reservoir solute mass fraction  $C_0$ . To this end, we have to specify the Damkhöler number  $Da$  and the efflorescence porosity  $\varepsilon$  in order to determine  $\lambda$  and  $\alpha$  from Eqs. (12) and (14). Although the determination of efflorescence porosity is still an open question, we have taken  $\varepsilon = 0.1$  since the porosity is *a priori* expected to be not too high. Regarding  $Da$ , we have tried the value of 4 used in Ref. 22.

As depicted in Fig. 7, a good trend is obtained, but the exclusion length is significantly underestimated for the greater reservoir ion mass fractions. According to Ref. 22,  $Da$  can be computed as

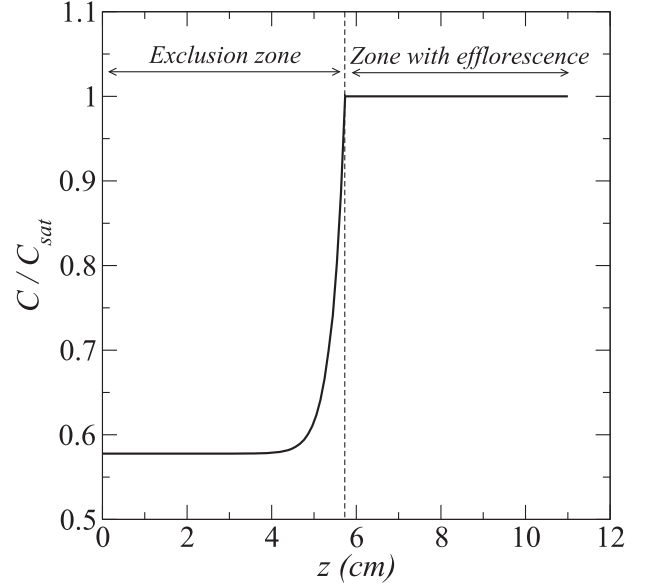




**FIG. 7.** Computed exclusion height as a function of the reservoir ion mass fraction. The red square symbols correspond to the experimental exclusion height determined as indicated in Table III and illustrated in Fig. 5. The blue circles correspond to the results of the 2D simulations (see Sec. V B) and the dashed lines to Eq. (16) for two values of the Damköhler number  $Da$ .

$Da = \sqrt{\frac{(1-\varepsilon)^2(1-C_{sat})k_r}{\varepsilon D_s^* a_v}}$ , where  $a_v$  is the pore wall surface area per unit volume and  $k_r$  is the precipitation coefficient ( $k_r \approx 2.3 \times 10^{-3}$  m/s<sup>23</sup>). As in Ref. 22, we assumed that  $a_v$  could be estimated as  $a_v = \frac{3(1-\varepsilon)}{r_b}$ , where  $r_b$  is an equivalent grain size. Since the efflorescence is not blocking in the experiment and looks a bit like small cauliflowers in some areas, it can be expected that the pores in the efflorescence are bigger than in the salt crust considered in Ref. 22 ( $r_b \sim 0.6 \mu\text{m}$ ). With  $r_b \sim 10 \mu\text{m}$  for instance, one obtains  $Da \approx 10$ , thus greater than in Ref. 22. We have interpreted this result as an indication that  $Da$  was probably greater in the case of our experiments than for the compact crust considered in Ref. 22. For sufficiently high  $Da$ , i.e., above about 50,  $\lambda$  and  $\alpha$  become essentially independent of  $Da$  (since the ratio  $\frac{Da}{1+Da} \approx 1$ ). If we assume that  $Da$  for our efflorescence is sufficiently large for  $\frac{Da}{1+Da} \approx 1$ , we obtain from Eq. (16) the results depicted in Fig. 7 ( $Da = 100$ ). As can be seen, greater exclusion lengths are obtained in the range of the greater values of  $C_0$ , and a quasi-linear variation of  $H_e$  with  $C_0$  is obtained as in the experiments.

However, the slope is different and greater than in the experiment. Nevertheless, since Eq. (16) is based on a simple mass balance and a slice average 1D solution, it can be reasonably concluded that the proposed approach captures the essential ingredients at play. In Fig. 7, we have indicated the predictions of the 2D model presented in Sec. V B (for the case where  $\frac{Da}{1+Da} \approx 1$ ). This model can be seen as a 2D version of the simpler 1D model leading to Eq. (16). However, the 2D model cannot be solved analytically. As can be seen from



**FIG. 8.** Typical average ion mass fraction profile along the sample height computed from Eq. (A11) in the Appendix for  $C_0 = 0.15$ .

Fig. 7, the consideration of the 2D model improves the comparison with the experiments.

Additional insights can be gained from the slice averaged ion mass profile depicted in Fig. 8 for the condition of experiment A3 ( $C_0 = 0.15$ ).

This profile was computed from Eq. (A11) in the Appendix. In the region where the efflorescence is present at the surface, i.e., for  $H_e \leq z \leq H$ ,  $C \approx C_{sat}$ . This is actually an assumption supported by the fact that the ion mass fraction in the efflorescence is the solubility mass fraction.<sup>22</sup> In the zone free of efflorescence, i.e.,  $0 \leq z \leq H_e$ , a typical exponential-like profile is obtained (as shown in the Appendix, it is not exactly exponential because the velocity decreases along  $z$ ). Based on previous studies, i.e., Ref. 11 and references therein, this type of profile is expected when the ion advection is noticeable compared to diffusion. Although the vertical velocity varies along  $z$  in our case, this can be evaluated from the Peclet number  $Pe = \frac{V_z(0)H_e}{\varepsilon_{pm}D_s^*}$ . For experiment A3, one obtains  $Pe \approx 29$ , thus greater than 1, which is consistent with the profile depicted in Fig. 8. Estimated values of  $Pe$  for all the samples are indicated in Table III.

This profile illustrates the fact that the ion mass fraction is lower than the solubility throughout the exclusion layer, consistent with the fact that no crystallization occurs in this zone.

## B. On the arch shape of the exclusion zone: Efflorescence boundary

As illustrated in Fig. 6, another intriguing feature of the exclusion zone is the arch shape of its upper boundary. It can be surmised that this has to do with either a greater evaporation flux on the edge or with the impact of the evaporation from the lateral faces or both. In any case, evaporation is greater in the region near the edge compared to the region of the front face away from the edges. In this

section, a 2D model is developed for computing this shape. Since the analysis presented in Subsection V A suggests that the system reaches a quasi-steady regime, steady-state equations are considered in what follows. The flow within the porous sample is modeled using Darcy's law considering only the viscous effects and the mass balance equation as follows:

$$\nabla \cdot (\rho \mathbf{V}) = 0, \quad (17)$$

$$\mathbf{V} = -\frac{K}{\mu} \nabla P, \quad (18)$$

where  $K$  is the porous sample permeability and  $\mu$  is the solution dynamic viscosity.

The boundary conditions at the evaporative surface read

$$\mathbf{V} \cdot \mathbf{n} = \frac{j}{\rho}, \quad (19)$$

where no efflorescence is present (exclusion zone) and

$$\mathbf{V} \cdot \mathbf{n} = \frac{(1 + \alpha)j}{\rho}, \quad (20)$$

where the efflorescence is present. At the top surface of the immersed region (which corresponds to the bottom surface of the computational domain), the pressure is specified:

$$P = P_{bot.} \text{ at } z = 0. \quad (21)$$

The solute transport governing equation reads

$$\nabla \cdot (\rho \mathbf{V} C) = \nabla \cdot (\rho \epsilon D_s^* \nabla C) - (1 - C) a_v \rho k_r (C - C_{sat}), \quad (22)$$

while the associated boundary conditions at the evaporative surface read

$$(\rho \mathbf{V} C - \nabla \cdot (\rho \epsilon D_s^* \nabla C)) \cdot \mathbf{n} = 0, \quad (23)$$

where the efflorescence is not present and

$$(\rho \mathbf{V} C - \nabla \cdot (\rho \epsilon D_s^* \nabla C)) \cdot \mathbf{n} = \lambda j, \quad (24)$$

where the efflorescence is present.<sup>22</sup> At the bottom surface of the computational domain, the bottom reservoir solute concentration is imposed, namely,

$$C = C_0 \text{ at } z = 0. \quad (25)$$

In order to obtain a 2D model, the abovementioned equations are averaged over the thickness  $e$  of the porous sample using the operator  $\langle \cdot \rangle = \frac{1}{e} \int_0^e dy$ .

This leads to

$$\frac{\partial}{\partial x} (\rho V_x) + \frac{\partial}{\partial z} (\rho V_z) - \rho V_y]_{y=0} = 0, \quad (26)$$

$$\frac{\partial}{\partial x} (\rho V_x) + \frac{\partial}{\partial z} (\rho V_z) = \Psi, \quad (27)$$

or after combination with Darcy's law,

$$\frac{\partial}{\partial x} \left( \rho \frac{K}{\mu} \frac{\partial P}{\partial x} \right) + \frac{\partial}{\partial z} \left( \rho \frac{K}{\mu} \frac{\partial P}{\partial z} \right) = -\Psi, \quad (28)$$

where

$$\Psi = -(1 + \alpha) \frac{j}{e}, \quad (29)$$

where the efflorescence is present and

$$\Psi = -\frac{j}{e}, \quad (30)$$

where there is no efflorescence. Boundary conditions (19)–(21) still apply on the boundary of the 2D computational domain now considered. The governing equation for the solute transport takes the following form:

$$\begin{aligned} \frac{\partial}{\partial x} (\rho V_x C) + \frac{\partial}{\partial z} (\rho V_z C) = & \frac{\partial}{\partial x} \left( \rho \epsilon D_s^* \frac{\partial C}{\partial x} \right) + \frac{\partial}{\partial z} \left( \rho \epsilon D_s^* \frac{\partial C}{\partial z} \right) + \Psi_s \\ & - \xi(C - C_{sat})(1 - C) a_v \rho k_r (C - C_{sat}), \end{aligned} \quad (31)$$

where

$$\Psi_s = -\frac{\lambda j}{e}, \quad (32)$$

where the efflorescence is present and

$$\Psi_s = 0, \quad (33)$$

where there is no efflorescence.

$\xi(C - C_{sat})$  is the Heaviside function. Thus, the source term  $-(1 - C) a_v \rho k_r (C - C_{sat})$  in Eq. (31) is present only where  $C \geq C_{sat}$ .

Boundary conditions (19)–(21) still apply but only on the lateral boundaries of the 2D computational domain.

Naturally, the main unknown is the position of the efflorescence boundary, which corresponds to the lower  $C_{sat}$  isoline in the computational domain. In order to determine this position, an iterative method is used. A first computation is performed assuming no efflorescence. This leads to an ion mass fraction field where the ion mass fraction is much above  $C_{sat}$  in many places. Then, the boundary conditions are modified depending on whether  $C \geq C_{sat}$  at the considered location. This process is repeated until stabilization of the region where  $C \approx C_{sat}$ . The solution was obtained using the commercial simulation software COMSOL Multiphysics.

The solution typically gives the 2D distribution of the thickness averaged ion mass fraction  $C$  over the computational domain. With this model, the efflorescence zone corresponds to the region where  $C \approx C_{sat}$ , whereas the exclusion zone corresponds to the region where  $C < C_{sat}$ . The obtained ion mass fraction fields so obtained are shown in Fig. 6 together with the experimental efflorescence distributions. As can be seen, the model captures quite well the arch shape of the exclusion zone upper boundary. The impact of the bottom reservoir ion mass fraction  $C_0$  on the spatial extension of the exclusion zone is well reproduced. As shown in Fig. 7 and reported in Table IV, the exclusion height  $H_e$  is quite well predicted for A4 and A5 but overestimated for A2 and A3.

**TABLE IV.** Efflorescence exclusion height  $H_e$  (cm). Comparison between the experimental measurement and the predictions of the 1D and 2D models in the limit of large  $Da$  for the four samples.

	A2 ( $C_0 = 0.1$ )	A3 ( $C_0 = 0.15$ )	A4 ( $C_0 = 0.2$ )	A5 ( $C_0 = 0.25$ )
$H_e$ (experiment)	6.5	5	3.5	2
$H_e$ (1D model)	8	5.9	3.4	0.8
$H_e$ (2D model)	7.3	5.9	3.3	2

Overall, the 2D model leads to a clear improvement compared to the simpler 1D model. Based on the impact of the Damkhöler number on the 1D results (Fig. 7), the comparison between the 2D model and the experimental results could be probably improved by playing with  $Da$  (here, we have only considered the case where  $Da$  is sufficiently large for  $\frac{Da}{1+Da} \approx 1$ ). However, we consider the results shown in Figs. 6 and 7 as sufficiently convincing within the framework of the assumptions and simplifications associated with the model.

## VI. DISCUSSION

To the best of our knowledge, there is no previous work presenting a model similar to the one presented in Sec. V B where the impact of the efflorescence development is taken into account through specific boundary conditions. Naturally, models taking into account the salt precipitation effect have been developed, e.g., Refs. 1 and 2, but the precipitation in this model typically occurs within the pores of the porous substrate. This corresponds to subflorescence formation and not to efflorescence formation. This is an important difference because the efflorescence typically grows at the surface of the porous medium and not within the pores of the porous substrate. Actually, some precipitation can also occur in the pores close to the surface. This phenomenon has not been taken into account in our model considering that the major mechanism was the efflorescence external growth.

The comparison between the two versions of the model (1D and 2D) and the experimental results is not perfect. The exclusion zone upper boundary arch shape is well reproduced by the 2D model, and the impact of the bottom reservoir ion mass fraction is well captured. However, the prediction of the exclusion zone extent is not very accurate. This could be explained by some assumptions made in the modeling. For instance, we have totally ignored the probable spatial variations of the evaporation flux over the sample surface. The inspection of the efflorescence in Fig. 6 suggests a greater evaporation flux in the bottom of the efflorescence region zone since the efflorescence is more developed in this region. Also, we have neglected the possible variations of the efflorescence properties over the surface, its porosity, for instance.

We know from previous studies, e.g., Ref. 15, that the efflorescence can also severely reduce the evaporation rate due to pore clogging within the efflorescence. This notably depends on the porous substrate pore sizes and the evaporative demand. Therefore, the situation could be different when the conditions are such that the

efflorescence formation reduces the evaporation rate significantly. In other words, our model does not take into account the possible salt precipitation within the efflorescence pores that can lead to efflorescence pore clogging. This was neglected on the ground that there is no noticeable effect of the efflorescence development on the evaporation rate in the experiment. A more refined approach would be to include this effect in the modeling so as to be able to deal also with situations where the efflorescence formation significantly reduces the evaporation.

The analysis and models make use of the efflorescence growth rate expression derived in a recent article.<sup>22</sup> In this respect, the present study can be seen as a reasonably successful test for this expression and, thus, the modeling of the efflorescence growth. However, this model was used considering a Damkhöler number value significantly greater than in Ref. 22. Consistent with previous studies, i.e., Ref. 15, this indicates that different efflorescence growth regimes exist depending on the conditions (evaporative demand, porous medium pore sizes, etc.). It is surmised that the regime observed in our experiment belongs to the same category as the “patchy” regime described in Ref. 15 where the efflorescence formation had a very little impact on the evaporation. This type of regime could correspond to relatively high Damkhöler numbers, whereas lower Damkhöler could characterize the regimes where the efflorescence formation does have a detrimental impact on the evaporation. In this respect, it would be interesting to study whether the exclusion zone still persists when the efflorescence severely reduces the evaporation. However, these considerations are mere speculations at this stage. Further work is needed to clarify the efflorescence typology and its relation with the Damkhöler number introduced in Ref. 22.

## VII. CONCLUSION

We have presented an experiment combining evaporation and wicking of a NaCl solution with significant efflorescence development. The experiment shows that the efflorescence does not fully colonize the surface of the porous sample exposed to evaporation. A zone at the bottom of the sample, referred to as the exclusion zone, remains free of efflorescence over the whole experiment duration. The exclusion extent increases when the solute concentration in the feeding bottom reservoir is decreased. A simple analysis using the efflorescence growth rate model developed in a previous study<sup>22</sup> shows that a quasi-steady situation can be reached where the incoming solute mass flow rate is balanced by the salt precipitation at the efflorescence surface. This model shows that the solute concentration is less than the solubility in the exclusion zone, consistent with the fact that no efflorescence forms in the exclusion zone. The model leads to a result consistent with the experiments. The impact of feeding reservoir solute concentration on the exclusion zone extent is reasonably well predicted.

The upper boundary of the exclusion zone is arch shaped. This shape is well reproduced from a model, which is essentially a 2D version of the simpler 1D model used to predict the extent of the exclusion zone analytically. The 2D model shows that the arch shape is a consequence of the greater evaporation in the region of the lateral sides compared to the more central region of the sample main surface.

Finally, the occurrence of the exclusion zone can be seen as a good test case for models. More generally, the modeling approach presented in the study is expected to help develop better models of salt transport with crystallization at the surface of porous media in relation with soil salinization issues or the salt weathering of porous materials, for instance.

## APPENDIX: 1D ANALYTICAL SOLUTION

Since the sample is relatively narrow, it is assumed that the ion mass fraction is very close to the solubility throughout the region where the efflorescence is present at the surface, i.e., for  $H_e \leq z \leq H$ . As a result, diffusion takes place only between the sample inlet where  $C = C_0$  and the top of the exclusion zone where  $C = C_{sat}$ .

Considering, for simplicity, the problem in 1D and assuming steady-state conditions, the equation governing the solute transport in the porous medium reads

$$V_z \frac{\partial C}{\partial z} = \epsilon_{pm} D_s^* \frac{\partial^2 C}{\partial z^2}. \quad (A1)$$

The velocity distribution along the  $z$  coordinate in the region  $0 \leq z \leq H_e$  is obtained from the mass balance,

$$Q(z + dz) = Q(z) - Pjdz, \quad (A2)$$

where  $Q$  is the mass flow rate through the porous sample cross section and  $P$  is the active perimeter, i.e., the perimeter where evaporation takes place. With the notations in Fig. 2(b),  $P = w + 2e$  since there is no evaporation from the back face. This leads to

$$\frac{\partial Q}{\partial z} = -Pjdz, \quad (A3)$$

which, after integration, yields

$$Q(z) = Q(H_e) + Pj(H_e - z). \quad (A4)$$

Dividing Eq. (A4) by the porous sample cross section surface area ( $A = we$ ) gives the velocity field in the region  $0 \leq z \leq H_e$ :

$$V_z(z) = V_z(H_e) + \frac{Pj}{A\rho}(H_e - z). \quad (A5)$$

Combining the abovementioned equations leads to

$$\frac{\partial^2 C}{\partial z^2} = \frac{V_z}{\epsilon D_s^*} = \frac{V_z(H_e)}{\epsilon D_s^*} + \frac{Pj}{A\rho \epsilon D_s^*}(H_e - z), \quad (A6)$$

from which one obtains

$$\log\left(\frac{\partial C}{\partial z}\right) = \left(\frac{V_z(H_e)}{\epsilon D_s^*} + \frac{PjH_e}{A\rho \epsilon D_s^*}\right)z - \frac{1}{2} \frac{Pj}{A\rho \epsilon D_s^*} z^2 + B, \quad (A7)$$

which leads to

$$\frac{\partial C}{\partial z} = B_1 \exp\left(\left(\frac{V_z(H_e)}{\epsilon D_s^*} + \frac{PjH_e}{A\rho \epsilon D_s^*}\right)z - \frac{1}{2} \frac{Pj}{A\rho \epsilon D_s^*} z^2\right). \quad (A8)$$

The boundary condition reads

$$C = C_{sat} \text{ at } z = H_e, \quad (A9)$$

$$C = C_0 \text{ at } z = 0. \quad (A10)$$

The distribution of  $C$  is, thus, given by

$$C(z) = C_0 + B_1 \int_0^z \exp\left(\left(\frac{V_z(H_e)}{\epsilon D_s^*} + \frac{PjH_e}{A\rho \epsilon D_s^*}\right)z - \frac{1}{2} \frac{Pj}{A\rho \epsilon D_s^*} z^2\right) dz, \quad (A11)$$

where  $B_1$  is given from (A9) by the equation

$$B_1 = \frac{C_{sat} - C_0}{\int_0^{H_e} \exp\left(\left(\frac{V_z(H_e)}{\epsilon D_s^*} + \frac{PjH_e}{A\rho \epsilon D_s^*}\right)z - \frac{1}{2} \frac{Pj}{A\rho \epsilon D_s^*} z^2\right) dz}. \quad (A12)$$

The solute diffusive flux at  $z = 0$  (inlet of the non-immersed region of the sample) can then be expressed as follows:

$$\phi_{diff} = -\rho \epsilon_{pm} D_s^* \frac{\partial C}{\partial z} = -\rho \epsilon_{pm} D_s^* B_1. \quad (A13)$$

Determining  $B_1$  for a given  $H_e$  requires determining  $V_z(H_e)$ . This velocity is obtained from Eq. (12) and a simple mass balance as follows:

$$\rho V_z(H_e) we = ((H - H_e)(w + 2e) + we)(1 + \alpha)j. \quad (A14)$$

## DATA AVAILABILITY

The data that support the findings of this study are available from the corresponding author upon reasonable request.

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